

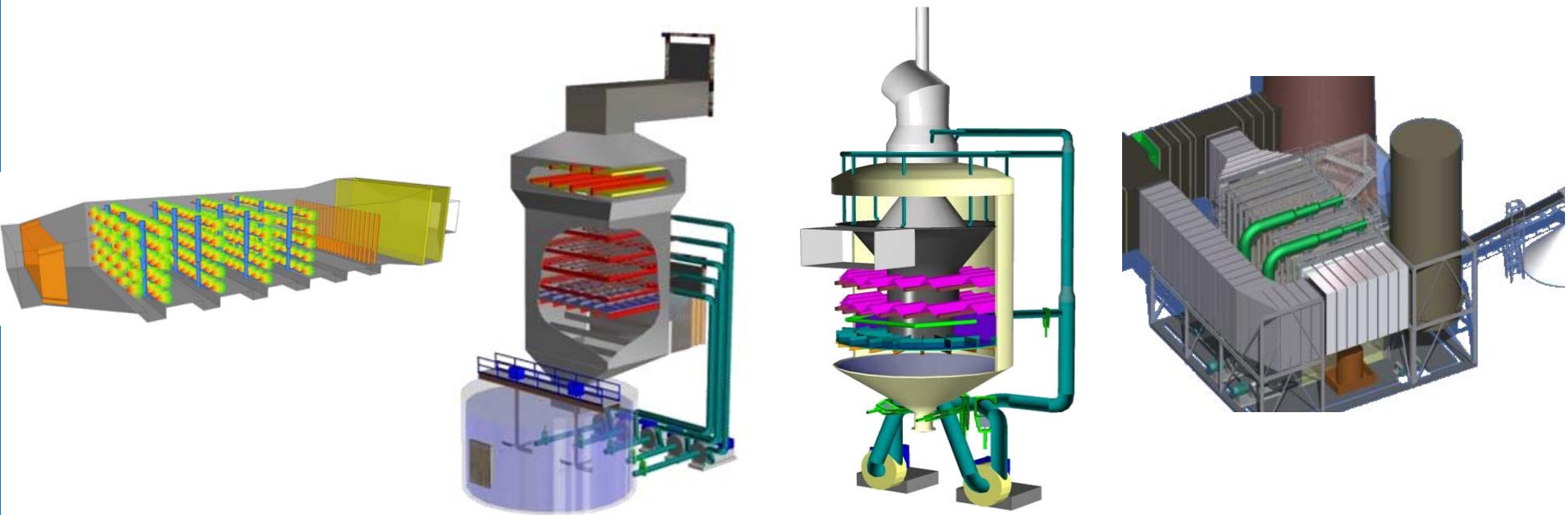
REINHOLD ENVIRONMENTAL Ltd.



2012 APC Round Table & Expo Presentation

July 16-17, 2012, in Baltimore, MD / Hosted by Duke Energy, Entergy,
FirstEnergy, Southern Company & TVA

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URS



Low Cost Wet FGD Upgrades for Complying with MATS Regulations

Presentation at:

2012 APC Round Table

Baltimore, MD

July 17, 2012

Workshop 17



Overview of MATS Regulations

	New Boilers		Existing Boilers	
	>8,300 Btu/lb	< 8,300 Btu/lb	>8,300 Btu/lb	< 8,300 Btu/lb
	lb/MM Btu	lb/MM Btu	lb/MM Btu	lb/MM Btu
PM	0.0050	0.005	0.03	0.03
SO ₂ (Surrogate for HCl)	0.04	0.04	0.20	0.20
Hg	1.0E-09	4.0E-06	1.0E-06	4.0E-06

- Covers all Electric Power Plants
 - Implementation by 2015
- PM limit is also a surrogate to HAP metals excluding Hg
 - Condensables such as SO₃ are excluded
- SO₂ limit is a surrogate for acid gases
- Proposed Hg limit for new boilers likely to be challenged

Overall Strategy for Compliance

- Unscrubbed Units:
 - DSI - option for plants firing low sulfur fuel which have efficient precipitators or bag houses
 - Low cost wet FGD (e.g., Co-Flo™) preferred option for plants with precipitators firing medium or high sulfur coal
 - CDS good option for plants which need new PM control systems
- Scrubbed Units:
 - Economics favor upgrade of wet FGD
 - Upgraded wet FGD systems provide multi-pollutant control and can be technology focal point for MATS compliance
 - SO₂
 - Hg
 - Particulate

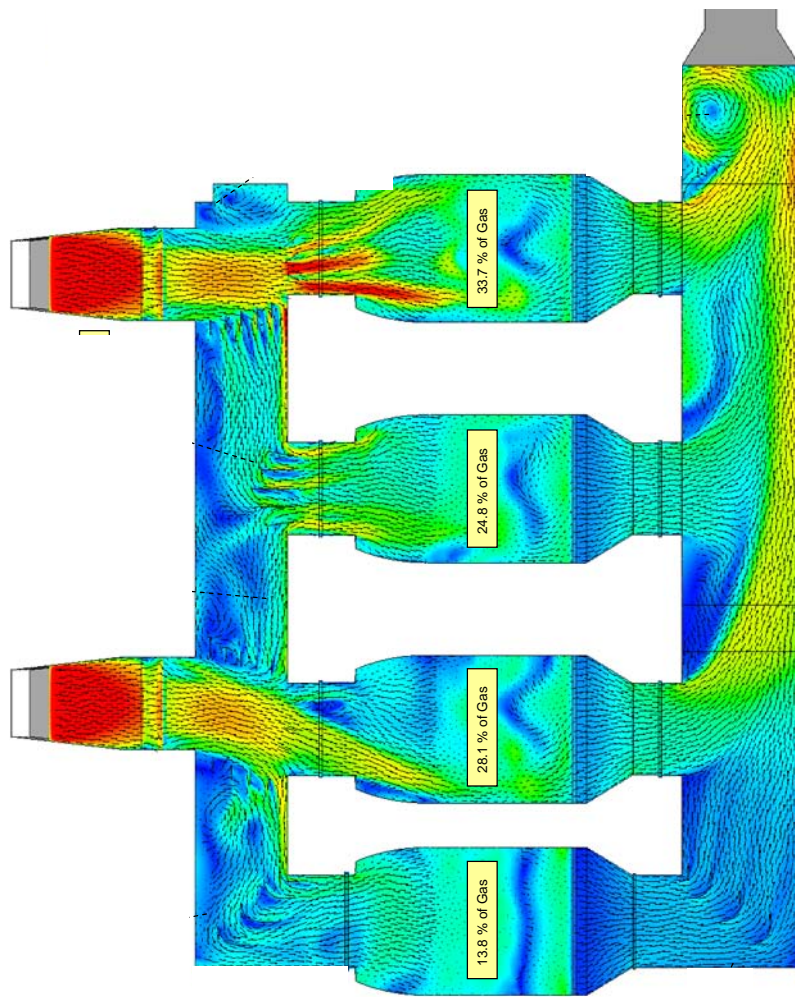
MATS Control Technology with Wet FGD

- 0.20 lb/MM Btu SO₂ can be achieved on all scrubber upgrade projects even with high sulfur coal
- Technology available to achieve high removal of oxidized Hg
 - Bromide addition
 - SCR catalysts being developed to enhance Hg oxidation
 - Additives available to minimize or eliminate re-emissions
- New technology to “polish” Hg removal downstream of wet FGD (e.g., Gore)
- High efficiency wet FGD can serve as a device to remove additional PM (polishing step)

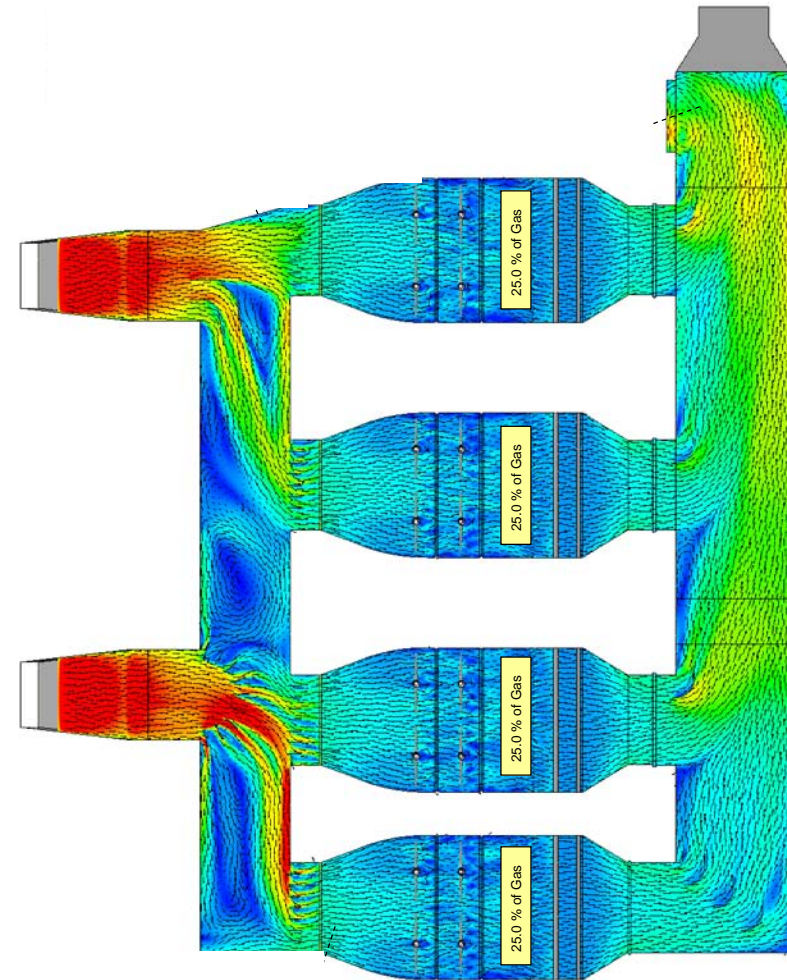
Typical Problems with Old Wet FGD Systems

- Gas Distribution among modules
- Gas Distribution inside absorber modules
- Poor spray coverage
- Wall sneakage
- Poor ME gas distribution
- Chemistry deficiencies

Unbalanced Flow Among Absorber Modules



Before Upgrade

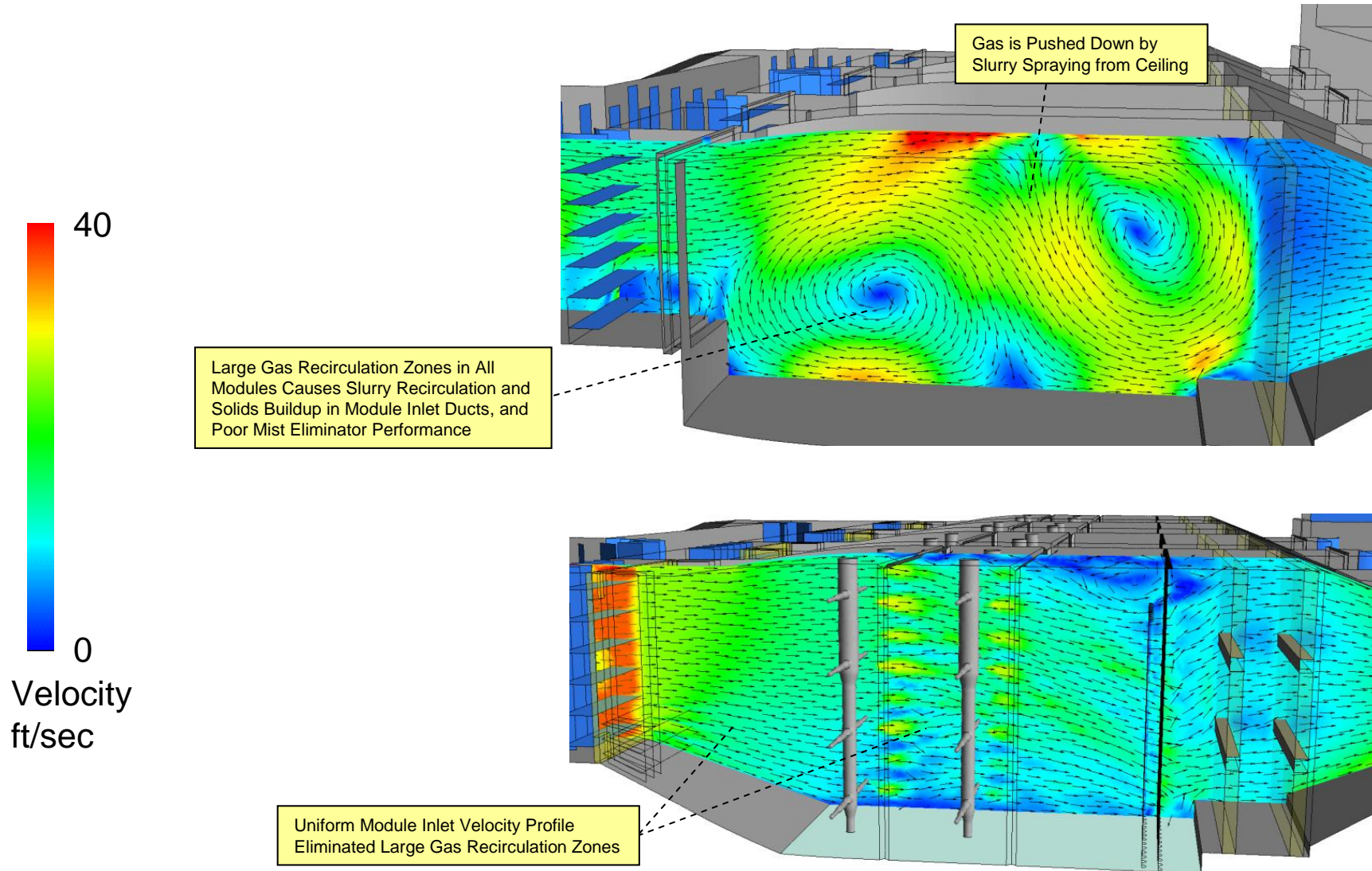


After Upgrade



Poor Gas Distribution

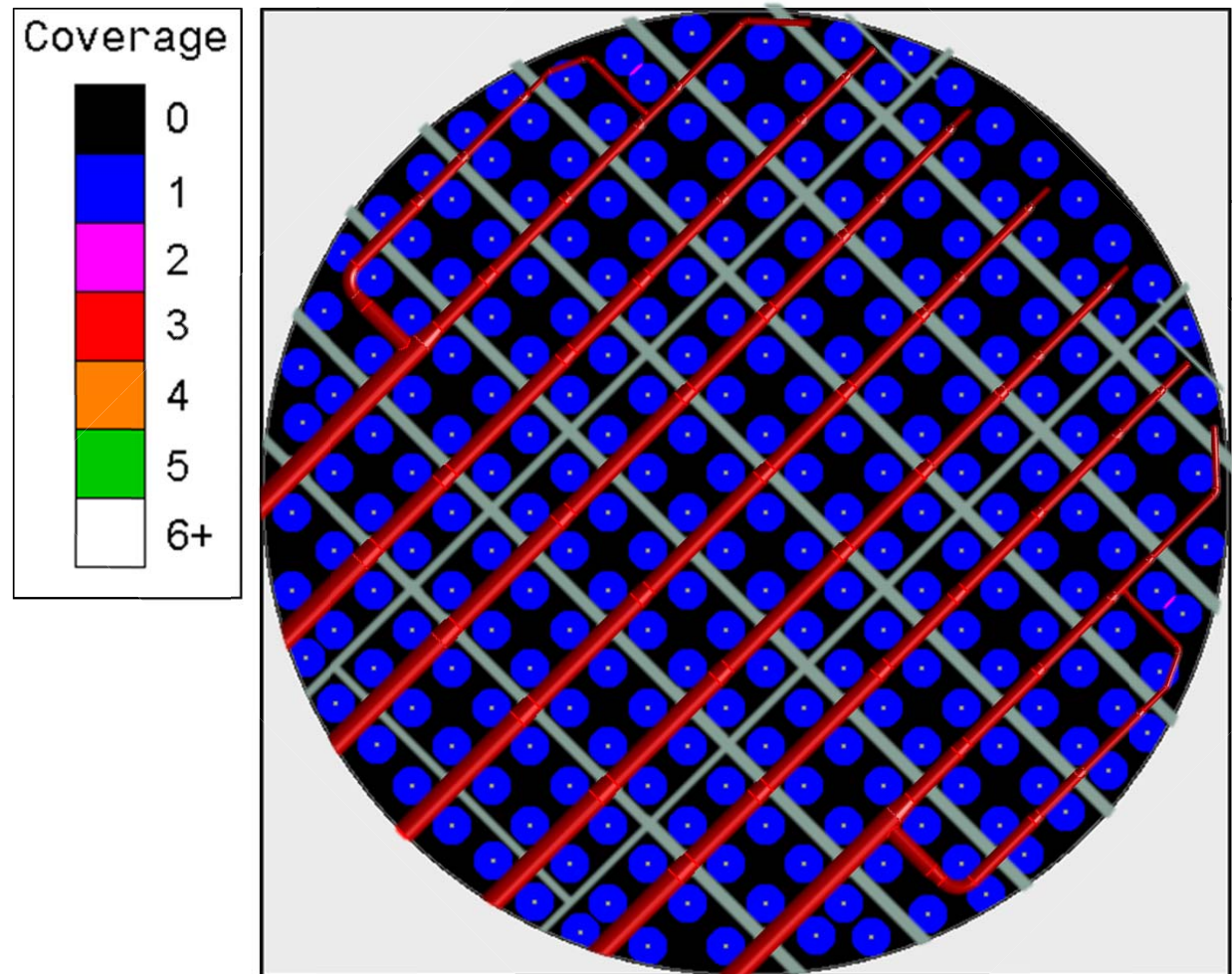
Case 1: Existing Crossflow Configuration, All Modules In Service



Case 2: Cocurrent Spray Conversion, All Modules In Service

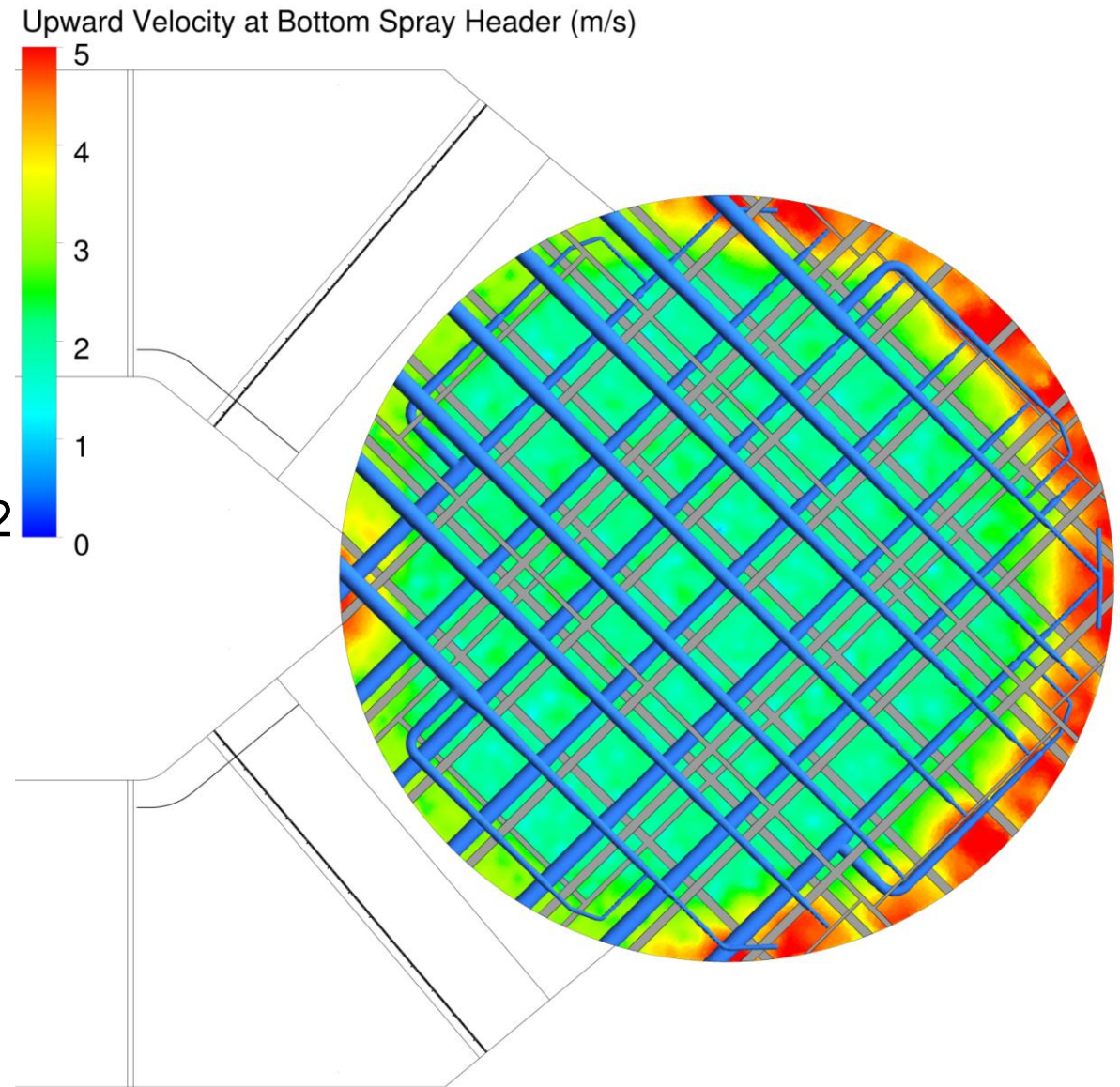
Poor Spray Coverage

- 39% spray coverage
- 90-degree spray nozzles
- Sneakage

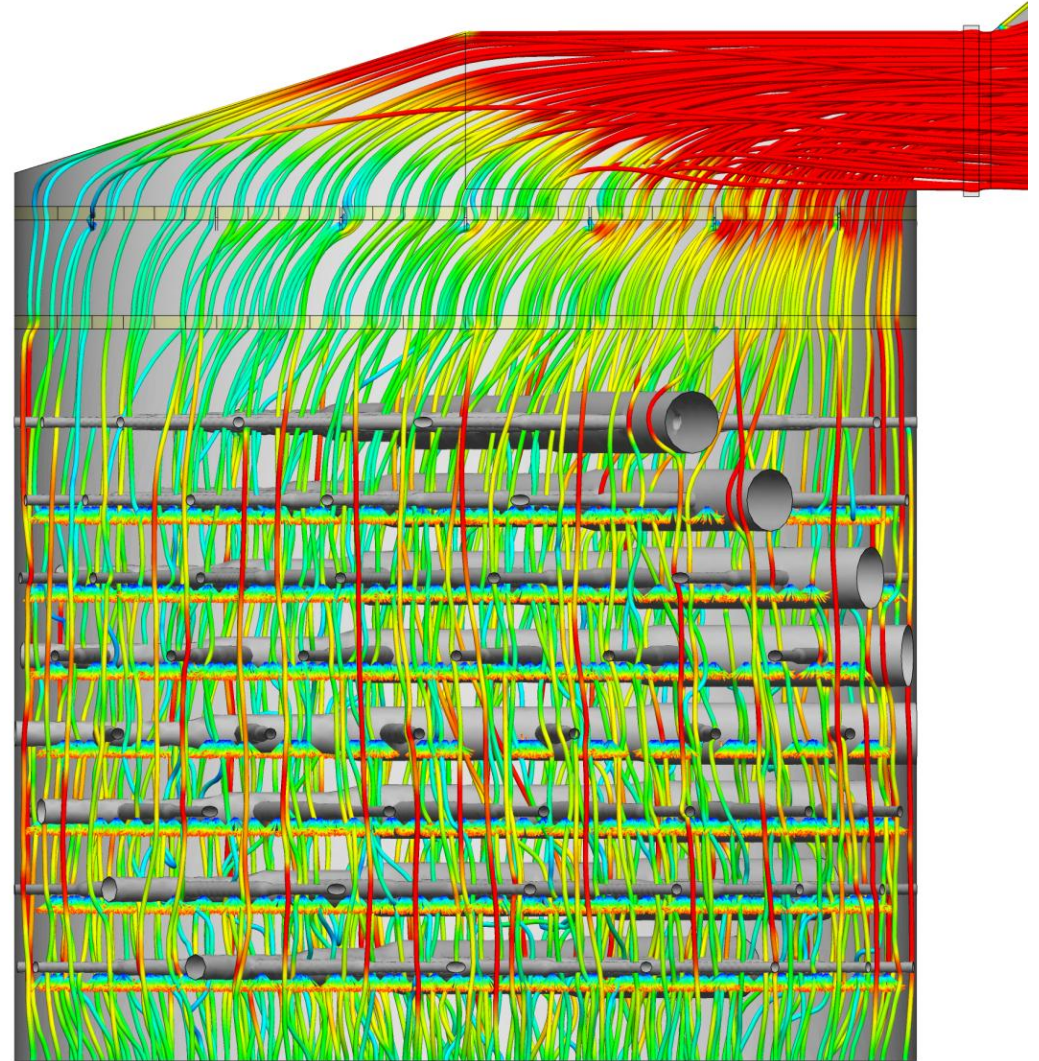
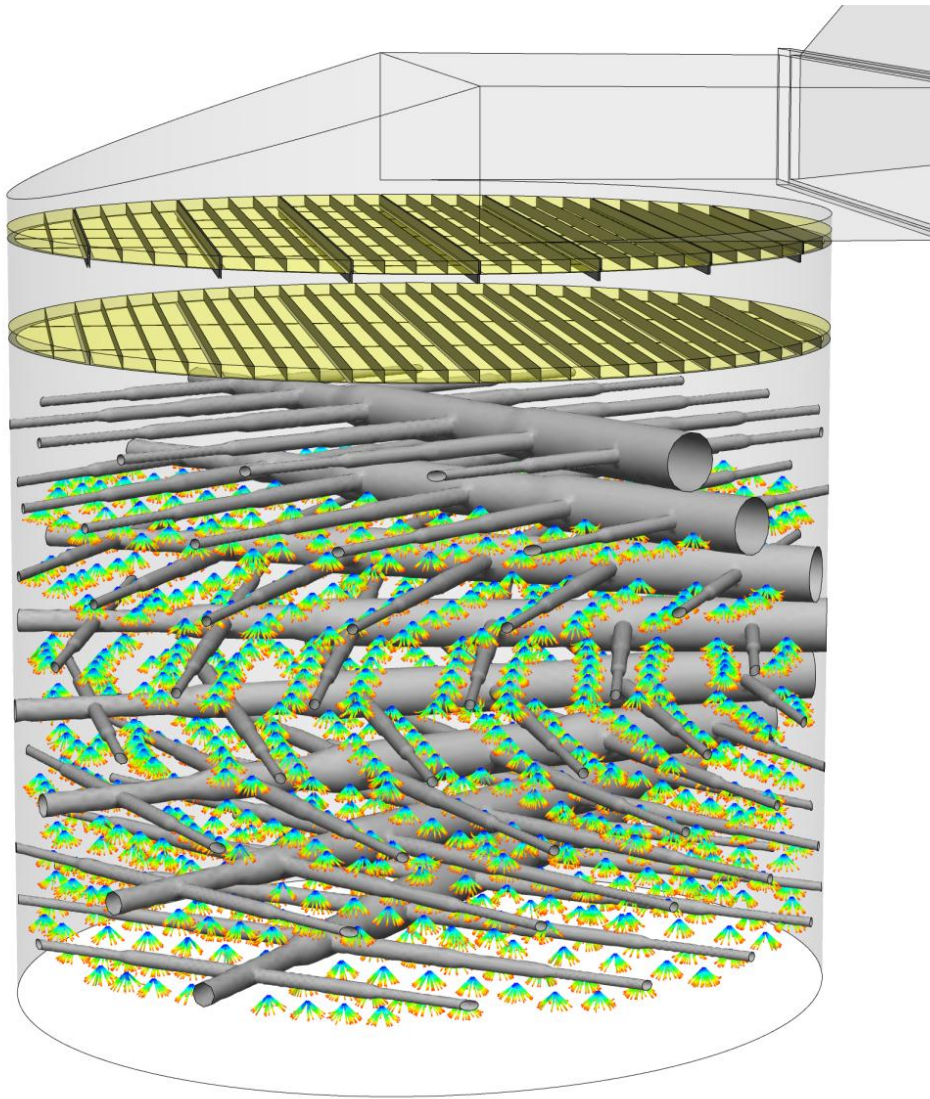


Wall Sneakage

- Poor spray coverage will lead to internal and peripheral gas sneakage
- Will often limit SO_2 removal to 95 percent regardless of pH and number of spray headers in service

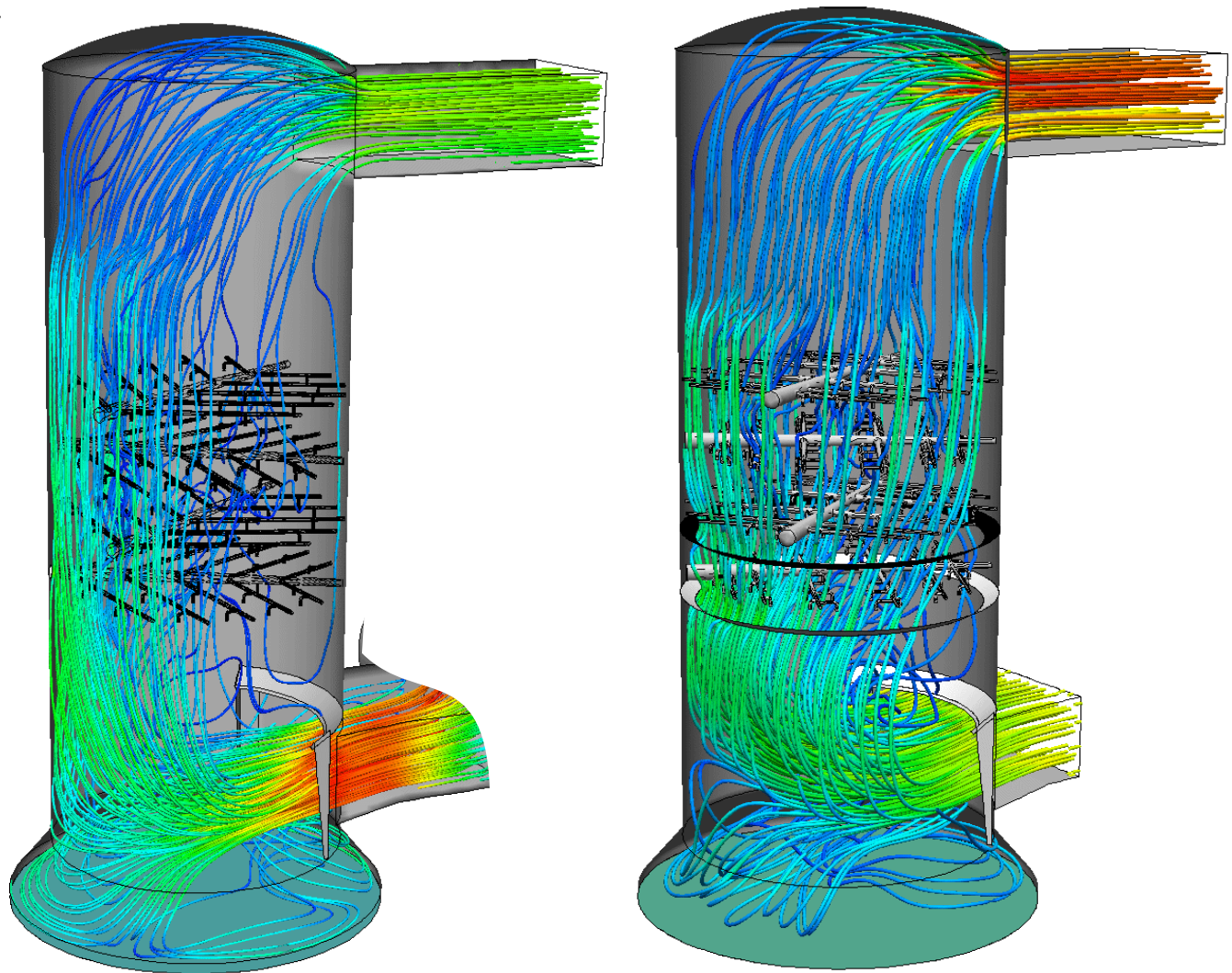


Poor Mist Eliminator Performance

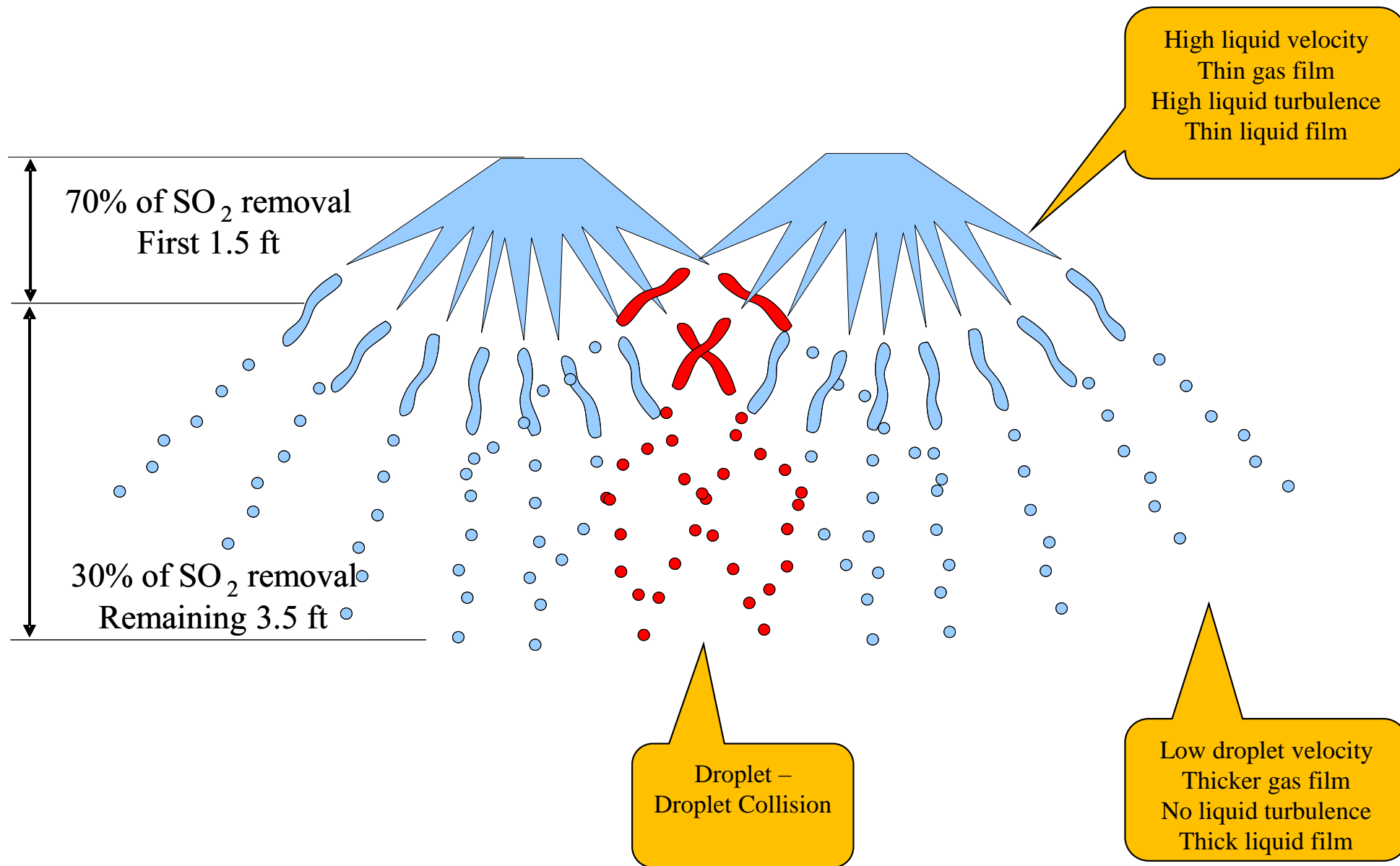


Available Tools

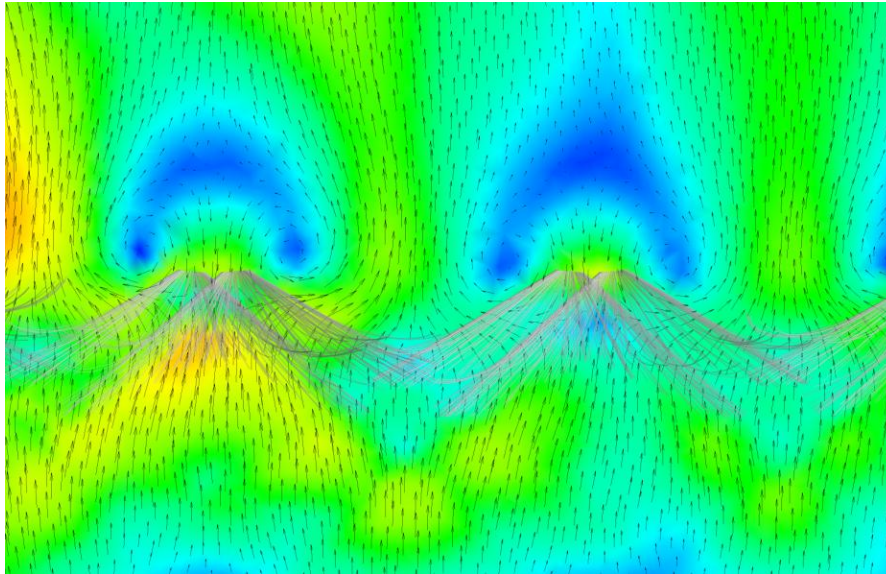
- Improved spray headers and spray nozzles
- Liquid distribution rings
- Dual-flow sieve trays
- Gore
- Modeling
 - CFD modeling
 - Process simulation modeling



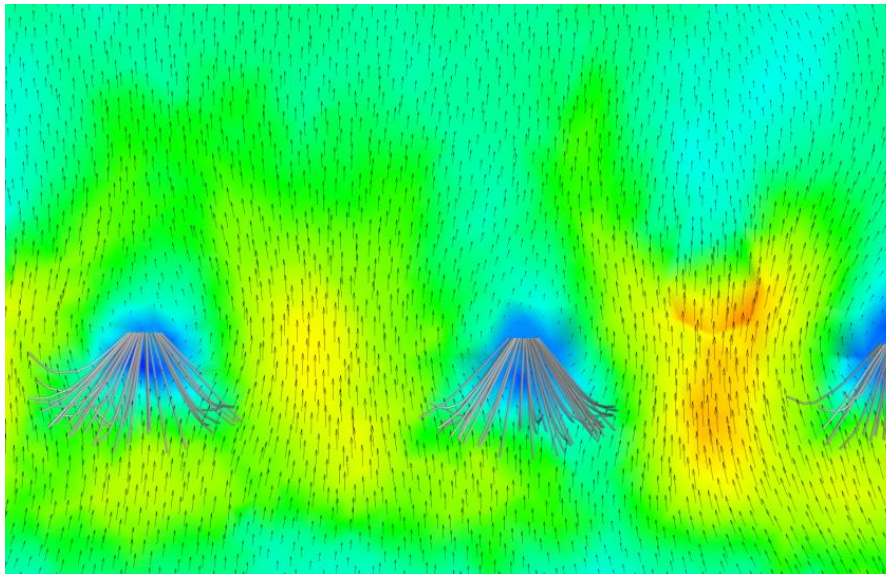
Nozzle Theory



Comparison of Hollow and Full Cone Nozzles

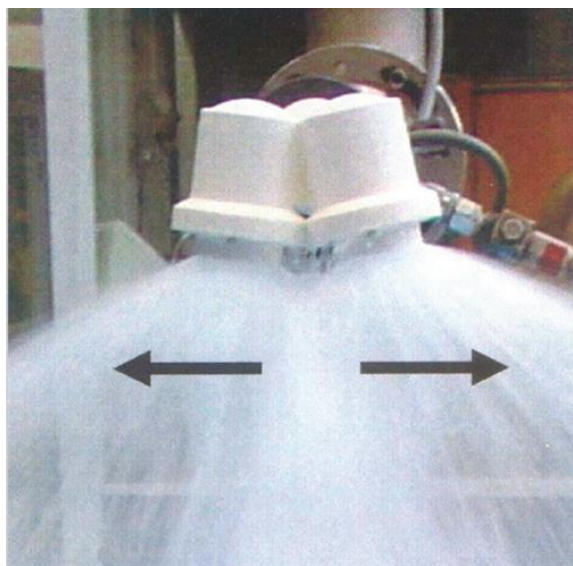


Hollow Cone
Spray

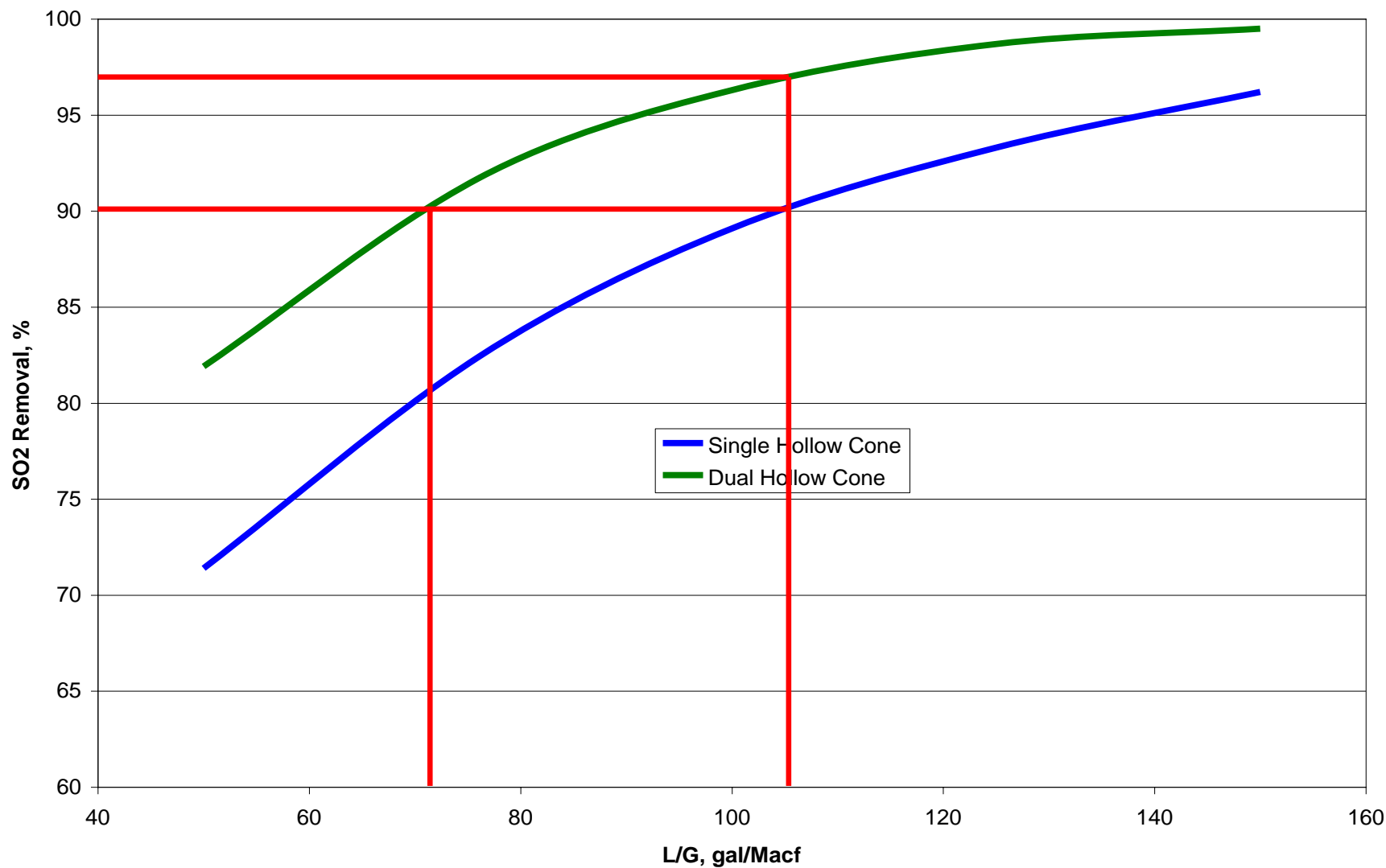


Full Cone Spray

Double Hollow Cone Spray Nozzle

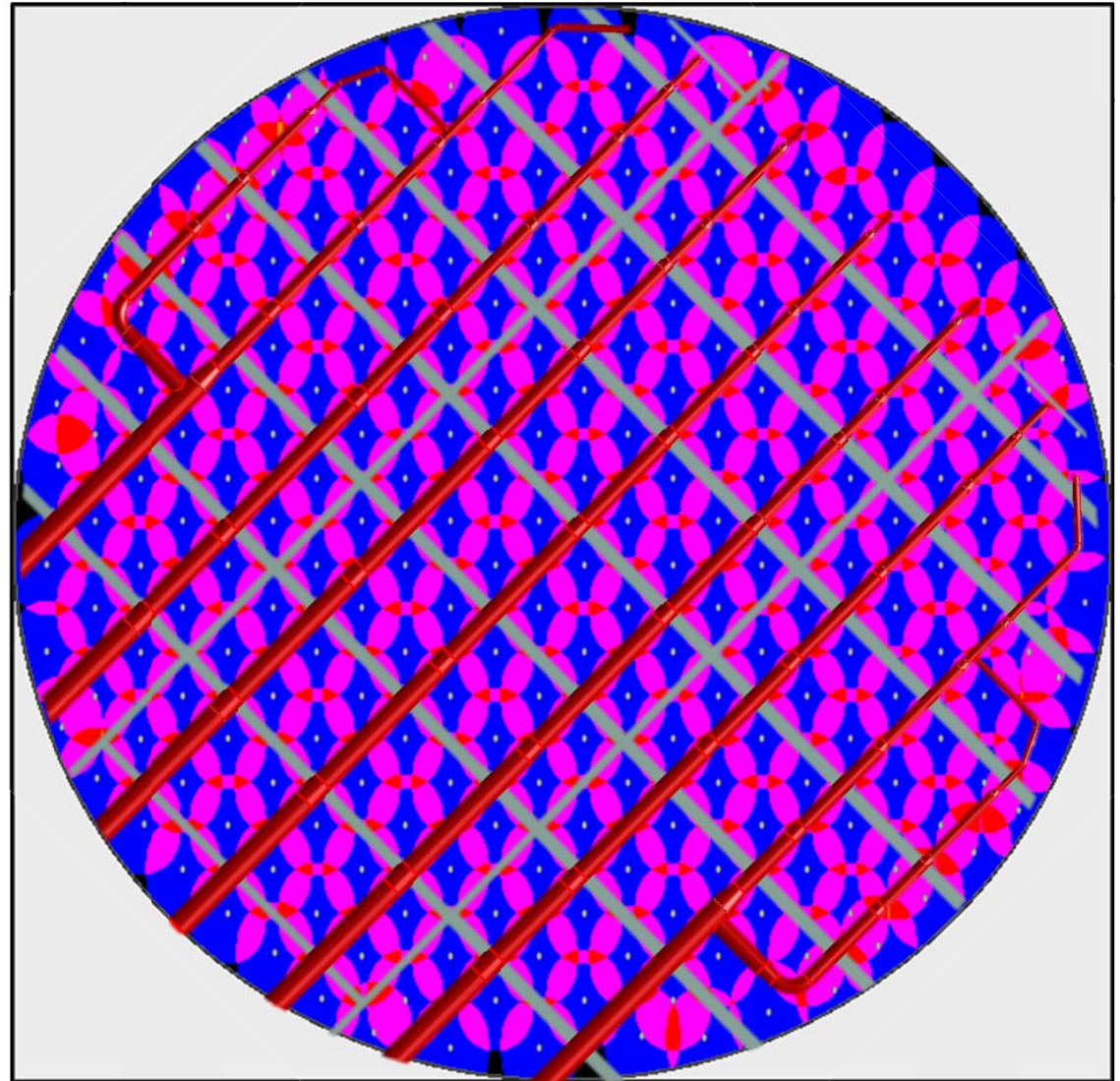
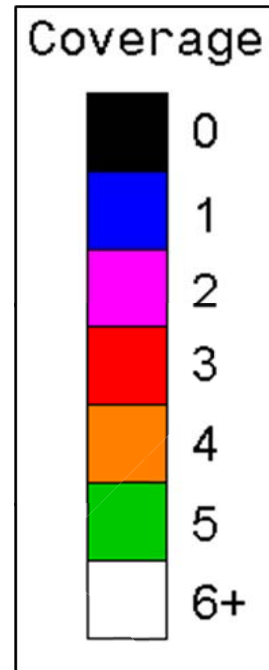


Comparison of SHC and DHC Spray Nozzles



High Efficiency Spray Header

- 165 % spray coverage
- 120-degree spray nozzles
- No sneakage



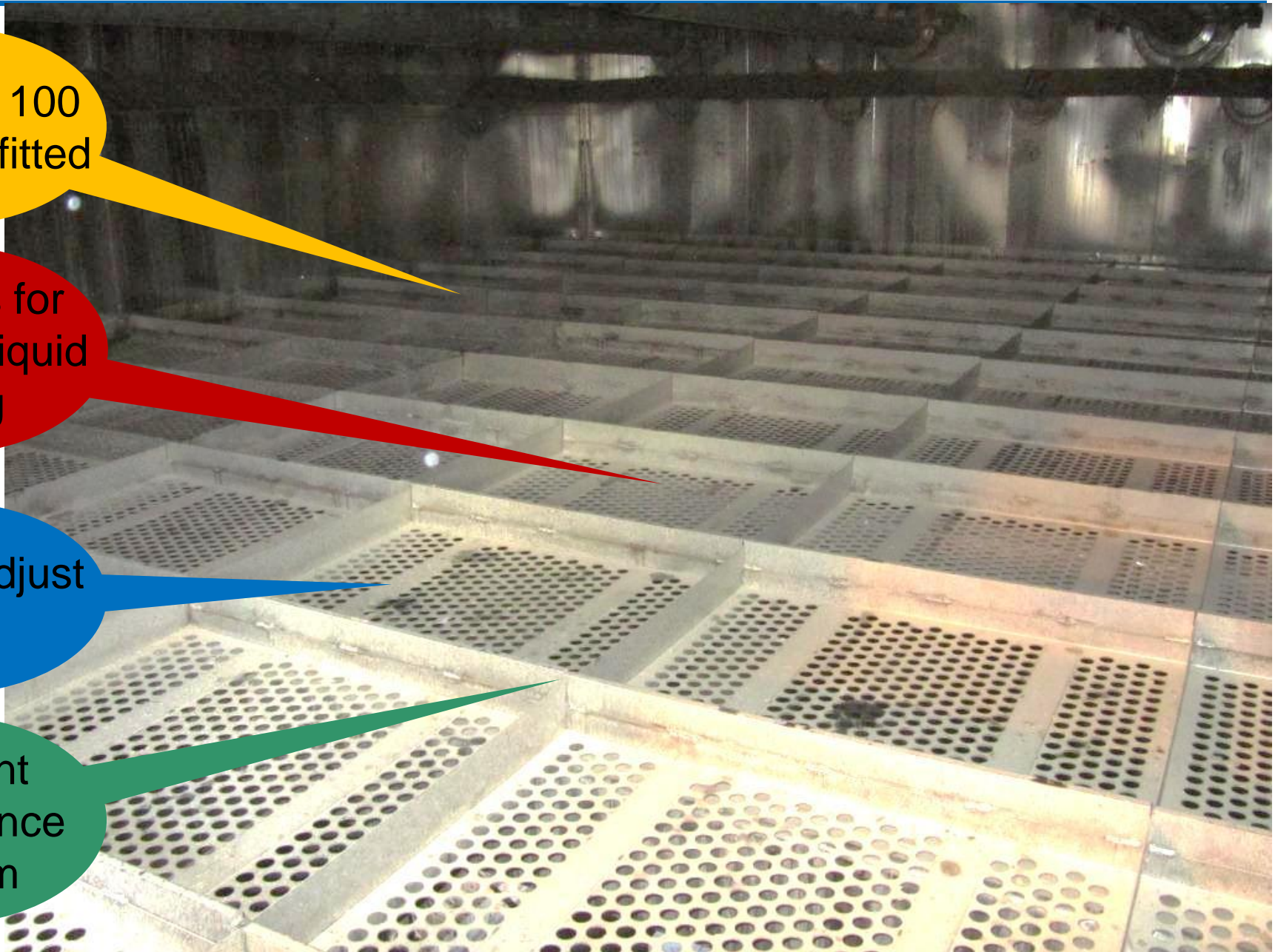
High Efficiency Tray

More than 100 trays retrofitted

Partitions for good gas liquid mixing

Strips to adjust dP

Excellent maintenance platform



Trays

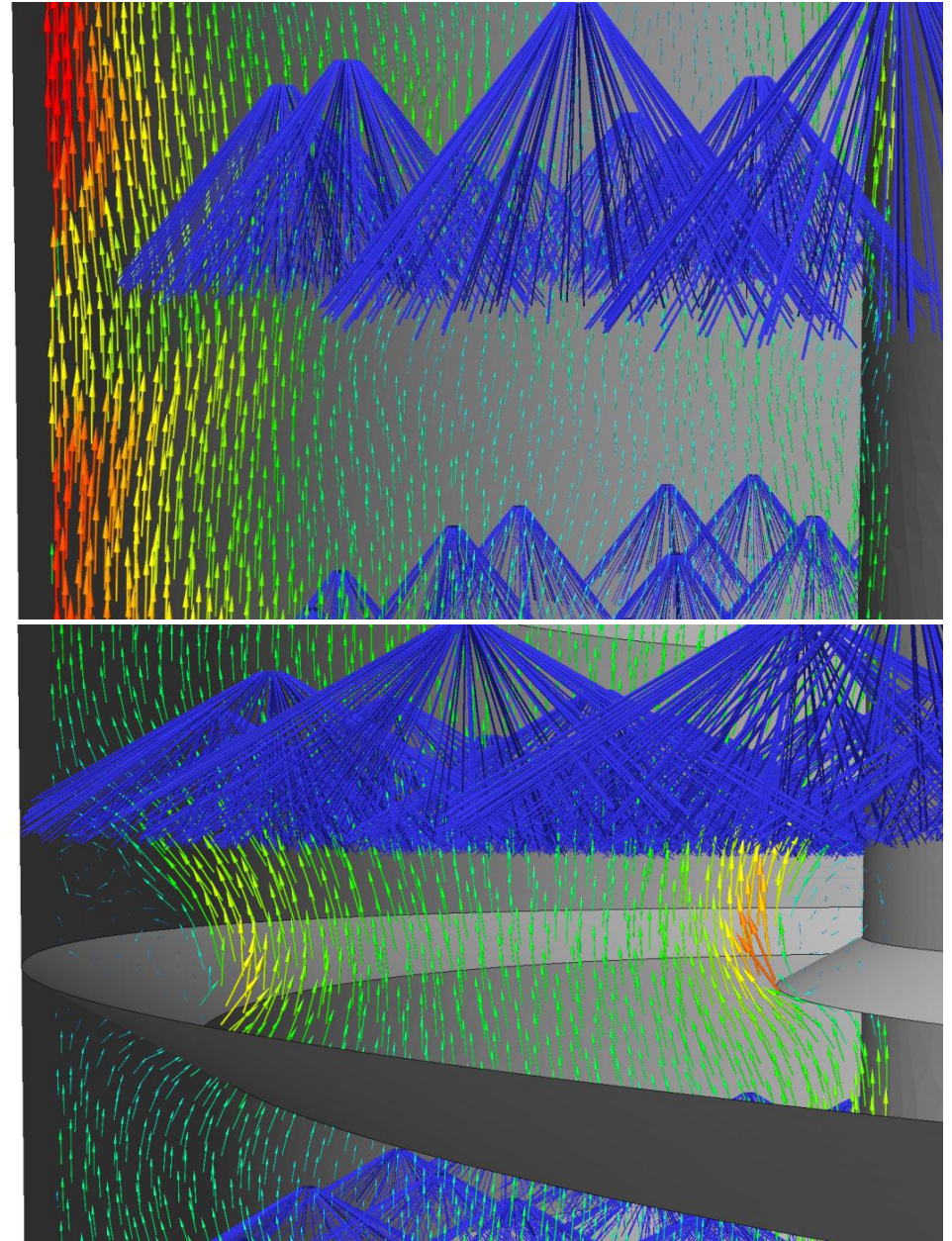
- Sieve Tray

- Great SO₂ removal device
 - Same SO₂ removal as one spray header
 - One or two per absorber
- Provides 50 Pa pressure drop
 - Correct gas distribution problems
 - Protects the inlet duct
 - Provides particulate removal
- Flexible Design
 - High velocity – hexagonal
 - Low velocity - round
- Can be used as Maintenance platform
- Stays clean



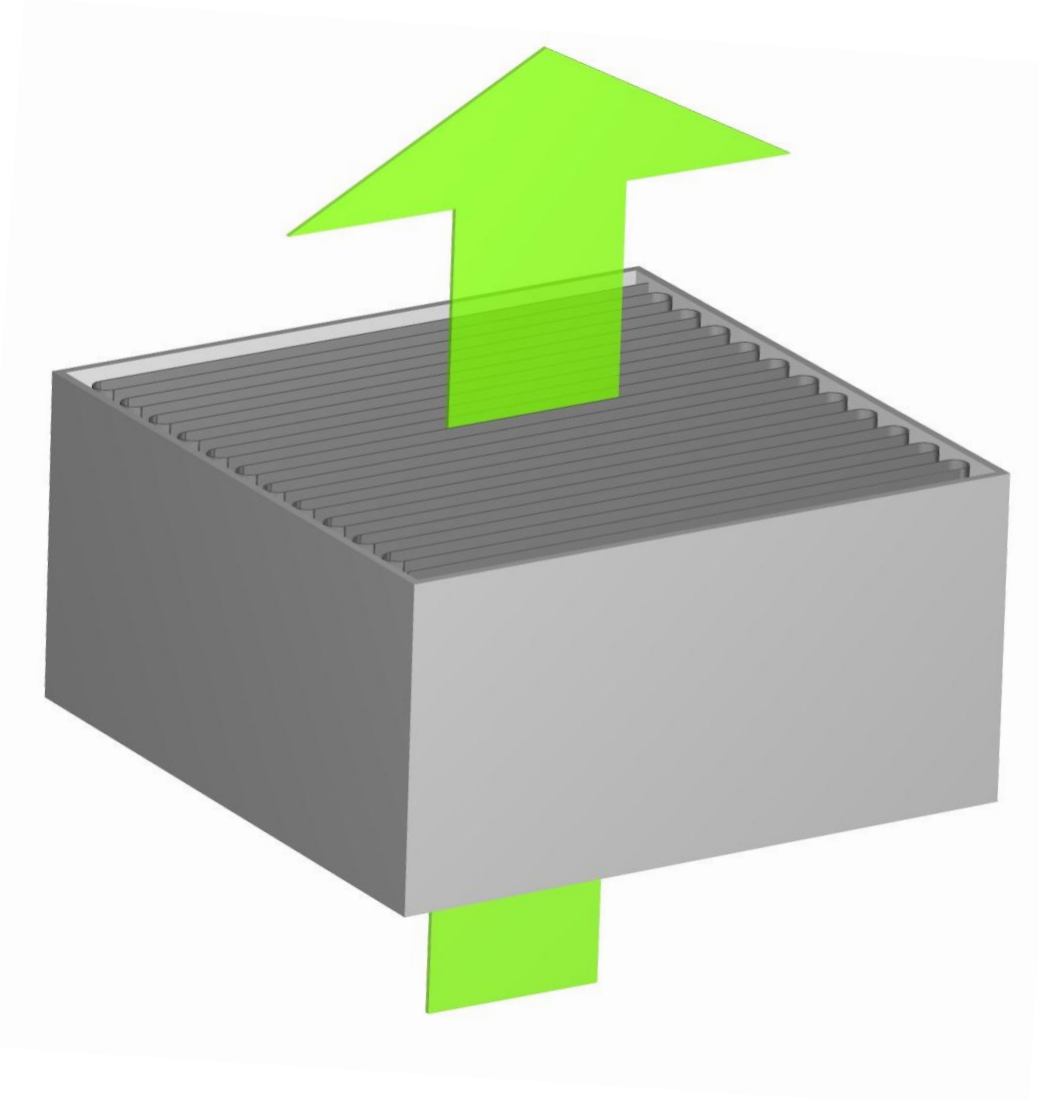
Wall Rings

- Designed to compensate for low spray density and high gas flow along absorber walls
- Rings are especially effective in small and/or rectangular modules
- Protects liner from wall erosion



Gore SPC Hg Control System

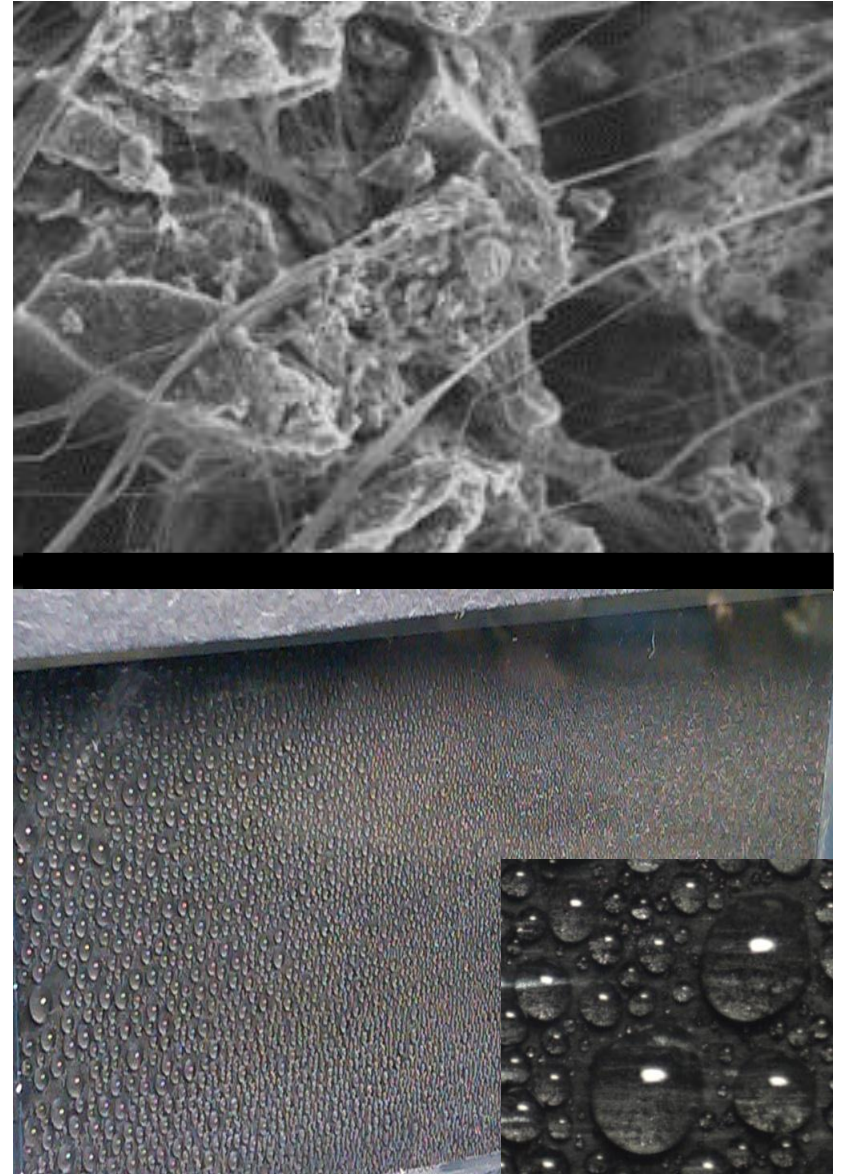
- Fixed Sorbent Technology
 - Located downstream of ME
 - Life expectancy multiple outage cycles.
- Pros
 - Low cost technology
 - Up to 90+ percent Hg removal
 - Up to 60+ percent SO₂ removal
 - Not sensitive to Hg concentration
 - Removes both ionic and elemental Hg
 - Not sensitive to Hg speciation
 - No additives to inject into the boiler
 - No activated carbon injection
 - No impact on the fly ash
 - No concerns regarding Hg reemission



Gore SPC Hg Control technology



- Fixed Bed Sorbent Polymer Composite (SPC) material
 - 1 ft wide tape of composite fluoropolymer membrane
 - Modularized
- Unique physical-chemical nature of the SPC material
 - Efficiently captures both elemental and oxidized mercury Hg
 - SO_2 is converted into sulfuric acid and expelled to SPC material's outer surfaces
 - Very high capacity for mercury storage
 - Does not require regeneration



Modular Structure

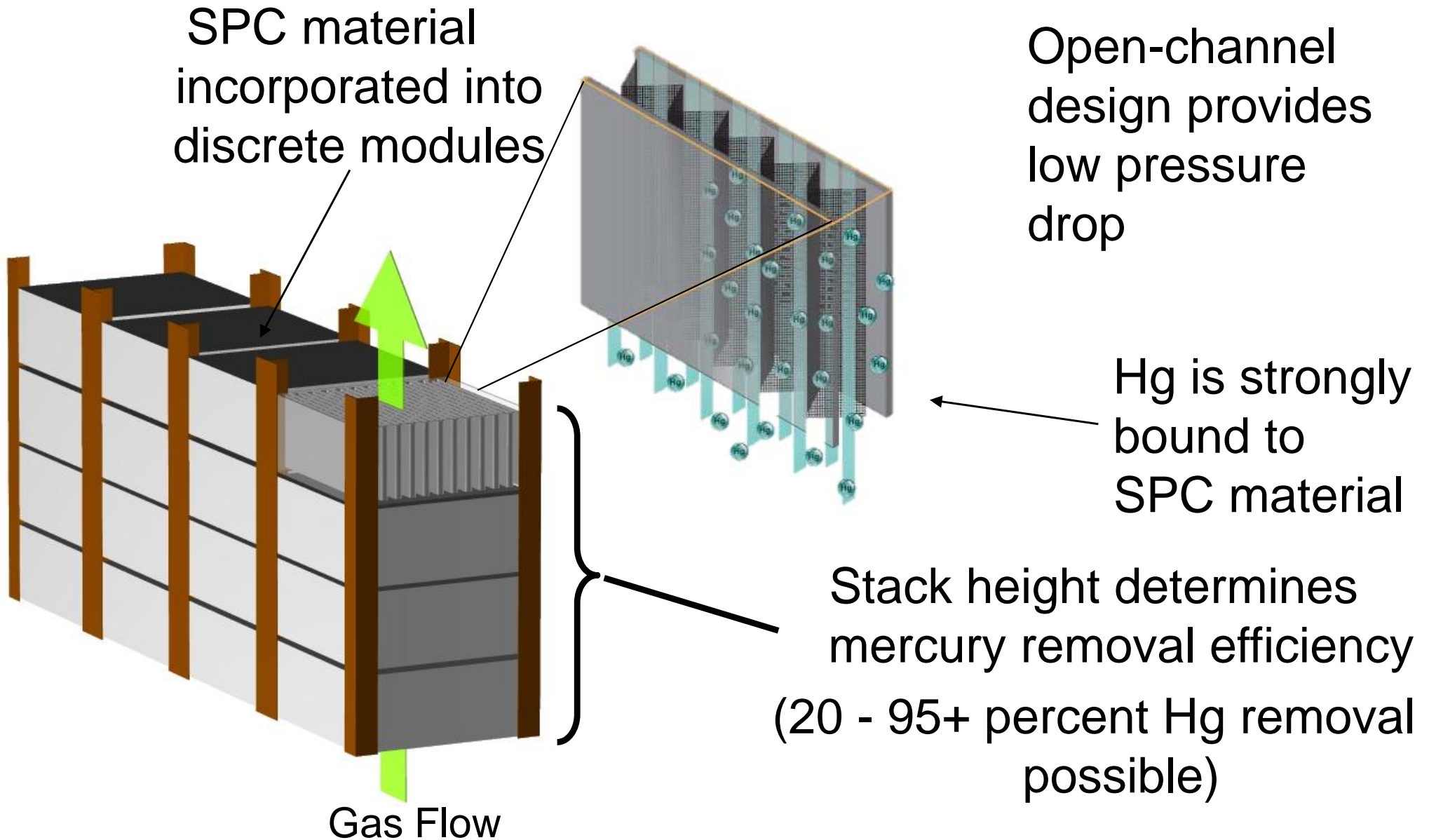
SPC material incorporated into discrete modules

Open-channel design provides low pressure drop

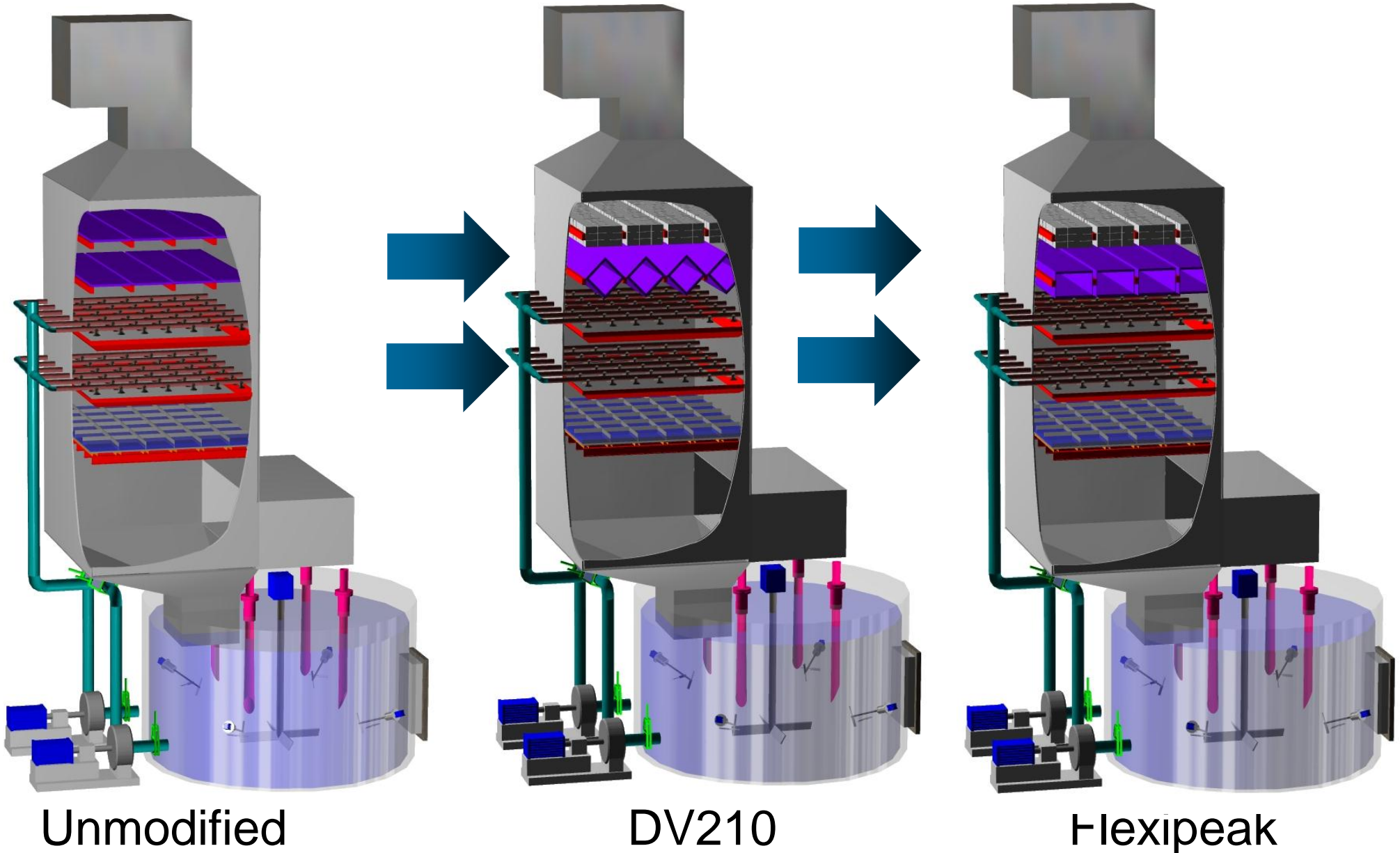
Hg is strongly bound to SPC material

Stack height determines mercury removal efficiency (20 - 95+ percent Hg removal possible)

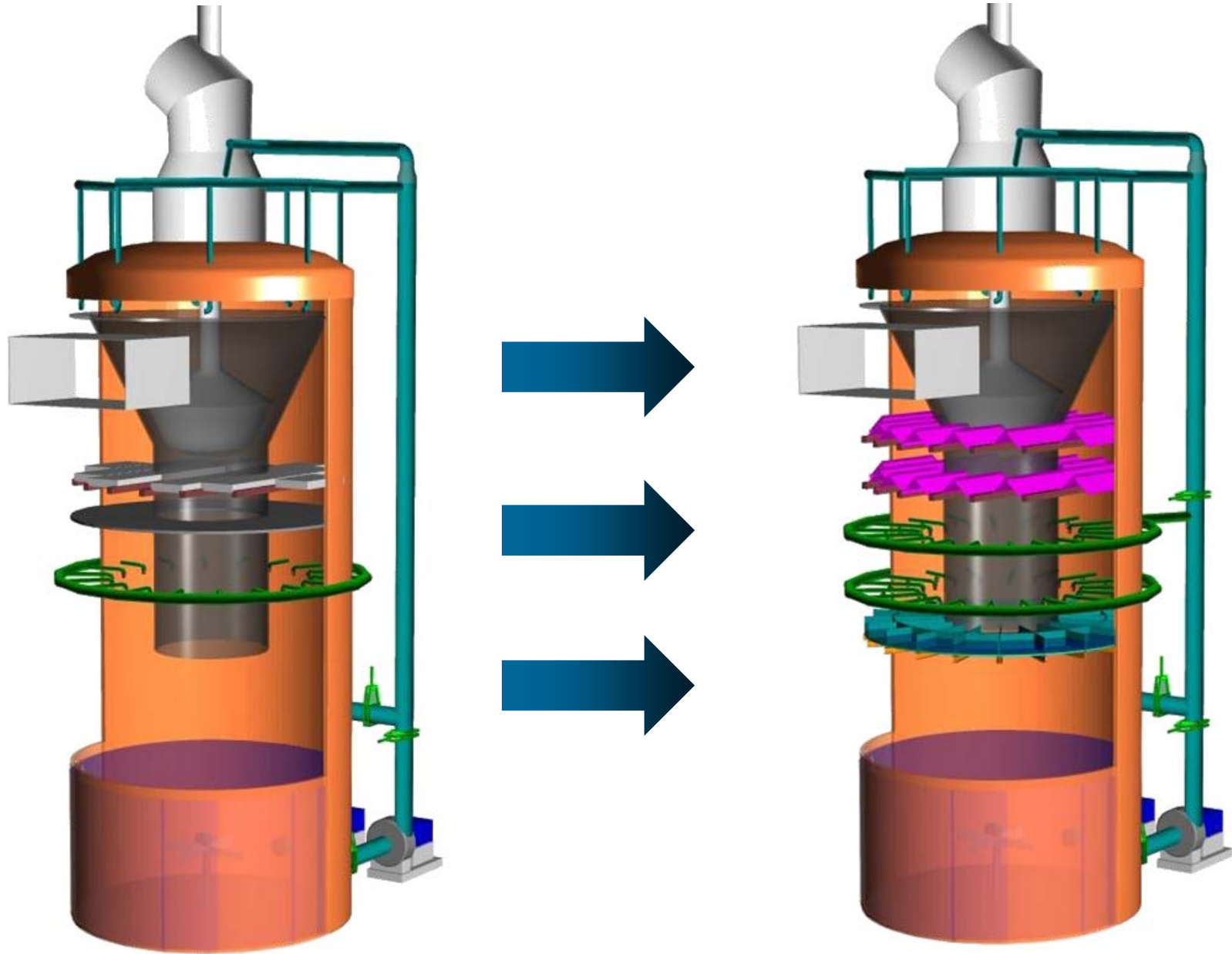
Gas Flow



Typical Installation

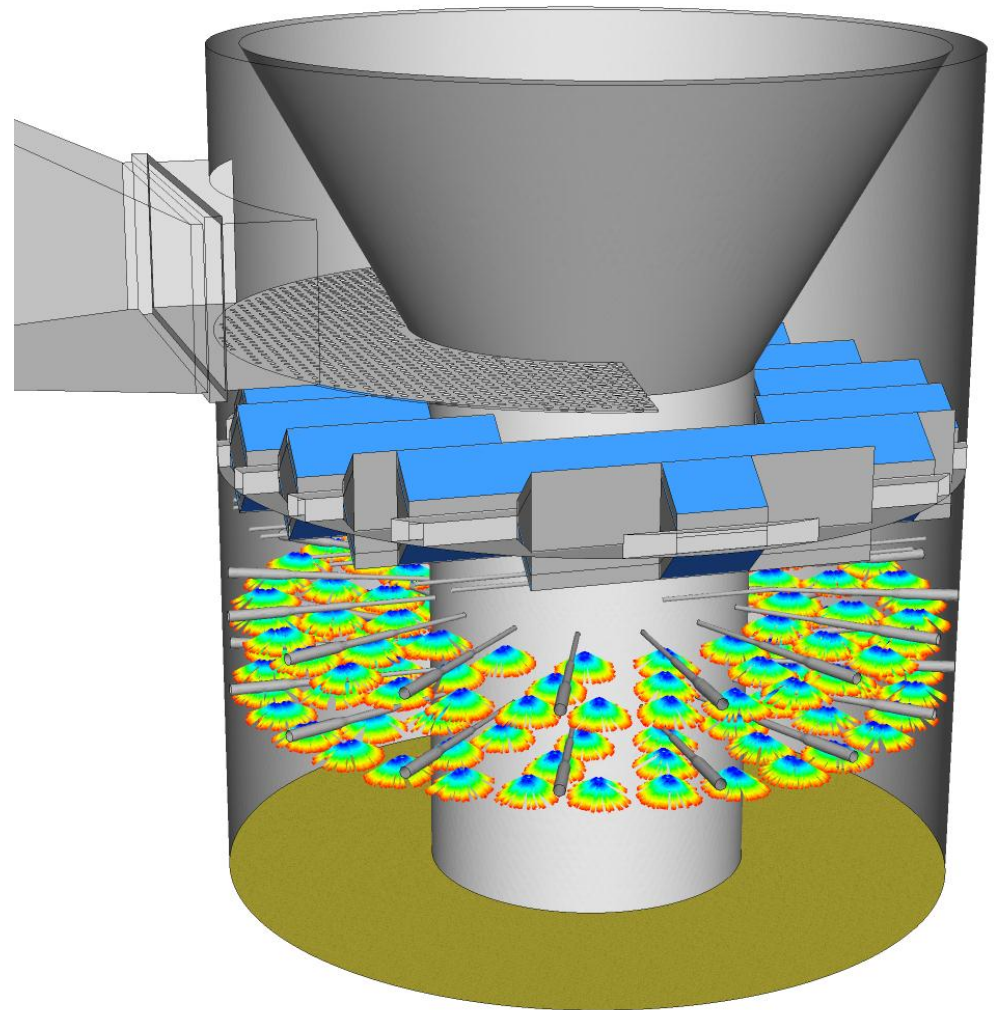


Venturi Fly Ash Scrubber

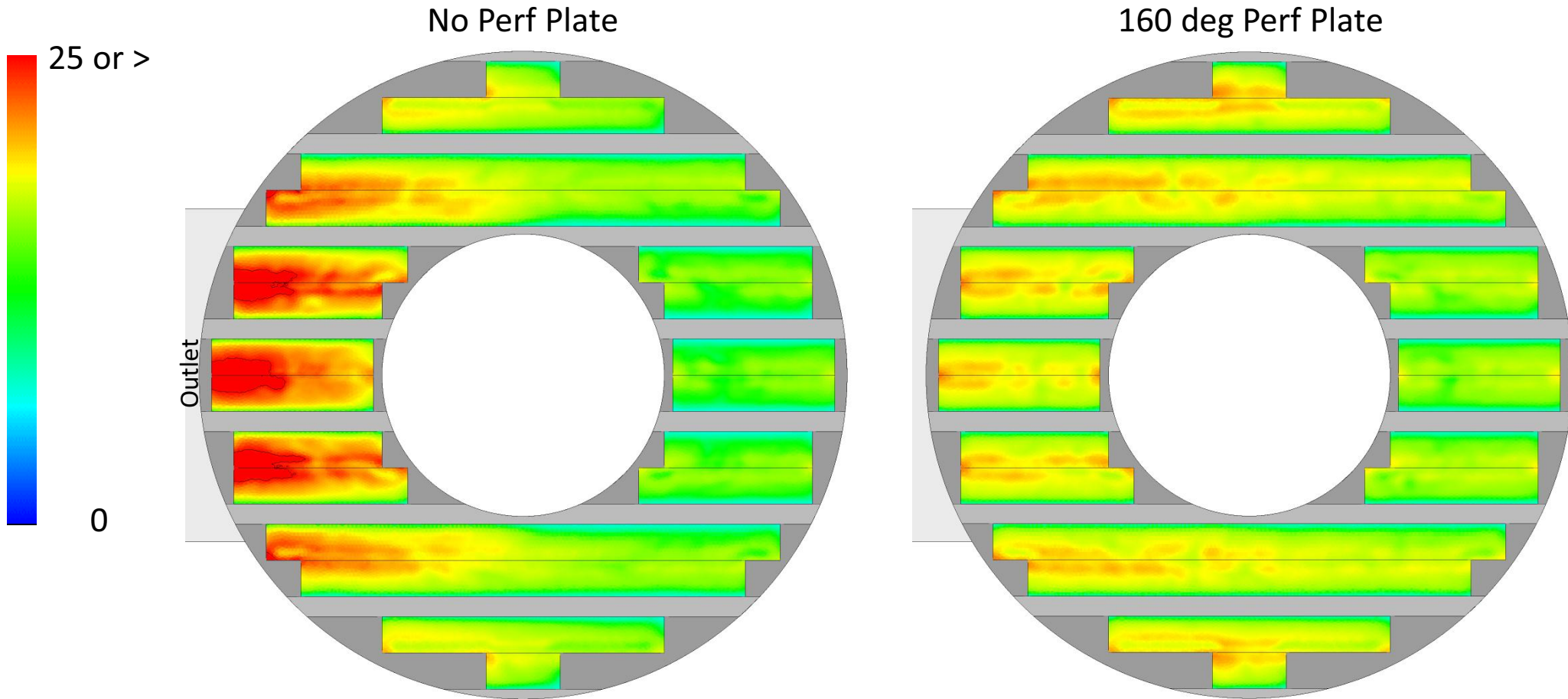


Upgrade Approach and performance

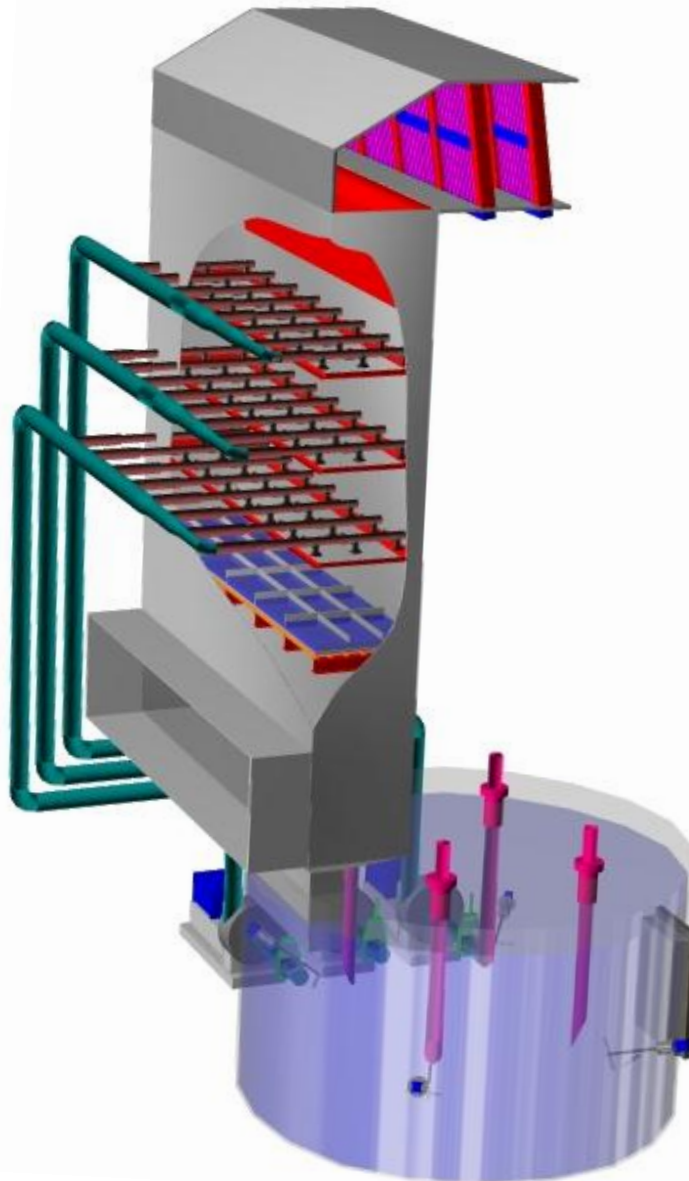
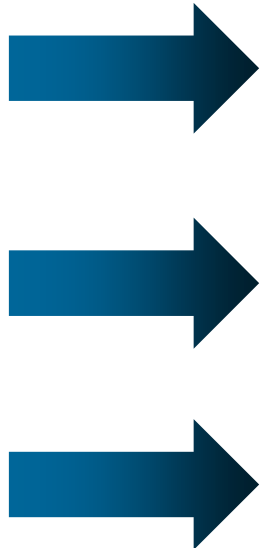
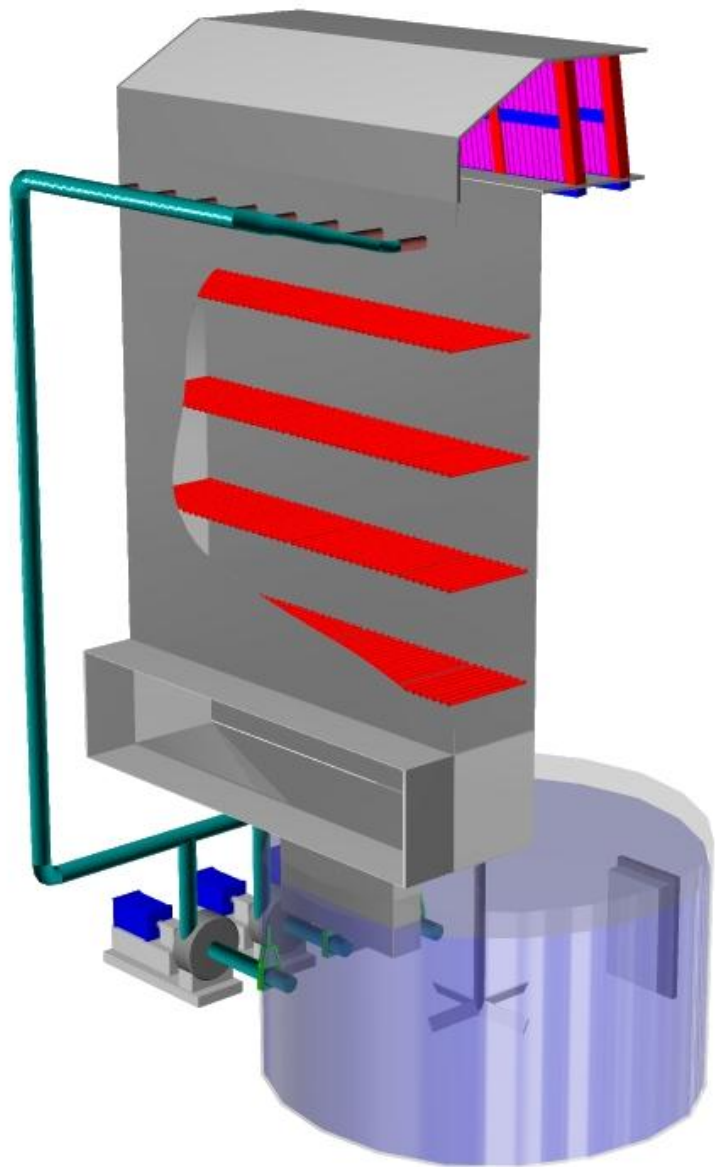
- Background
 - CEA scrubber
 - 1985
 - Medium sulfur coal
- Approach
 - Tray
 - Spray header
 - DHC spray nozzles
 - DV210 mist eliminator
 - Perforated plate
- Performance
 - Increased SO₂ removal from 80 percent to 98 percent
 - Decreased particulate emissions



Mist Eliminator Gas Distribution

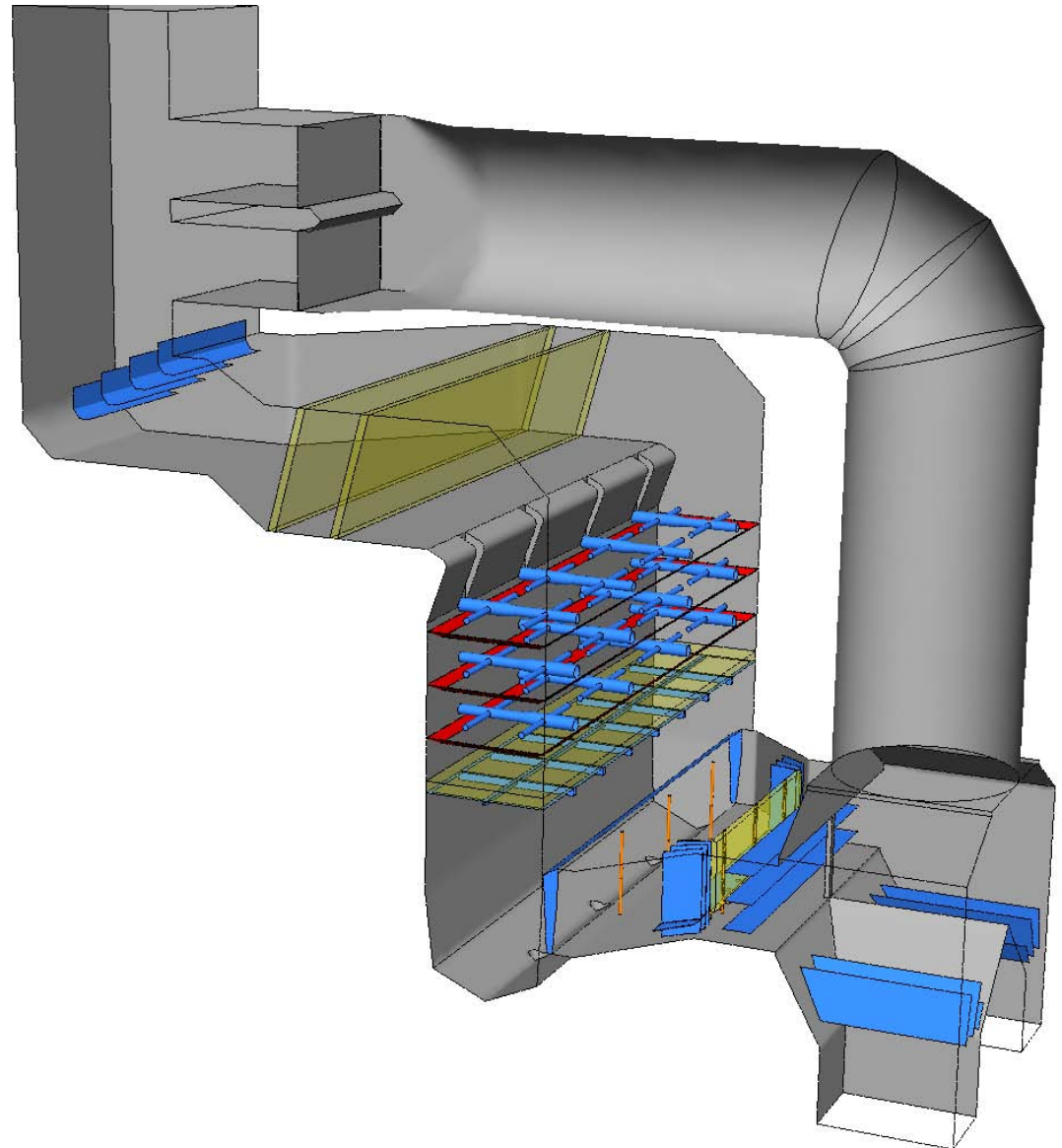


Rod Scrubber

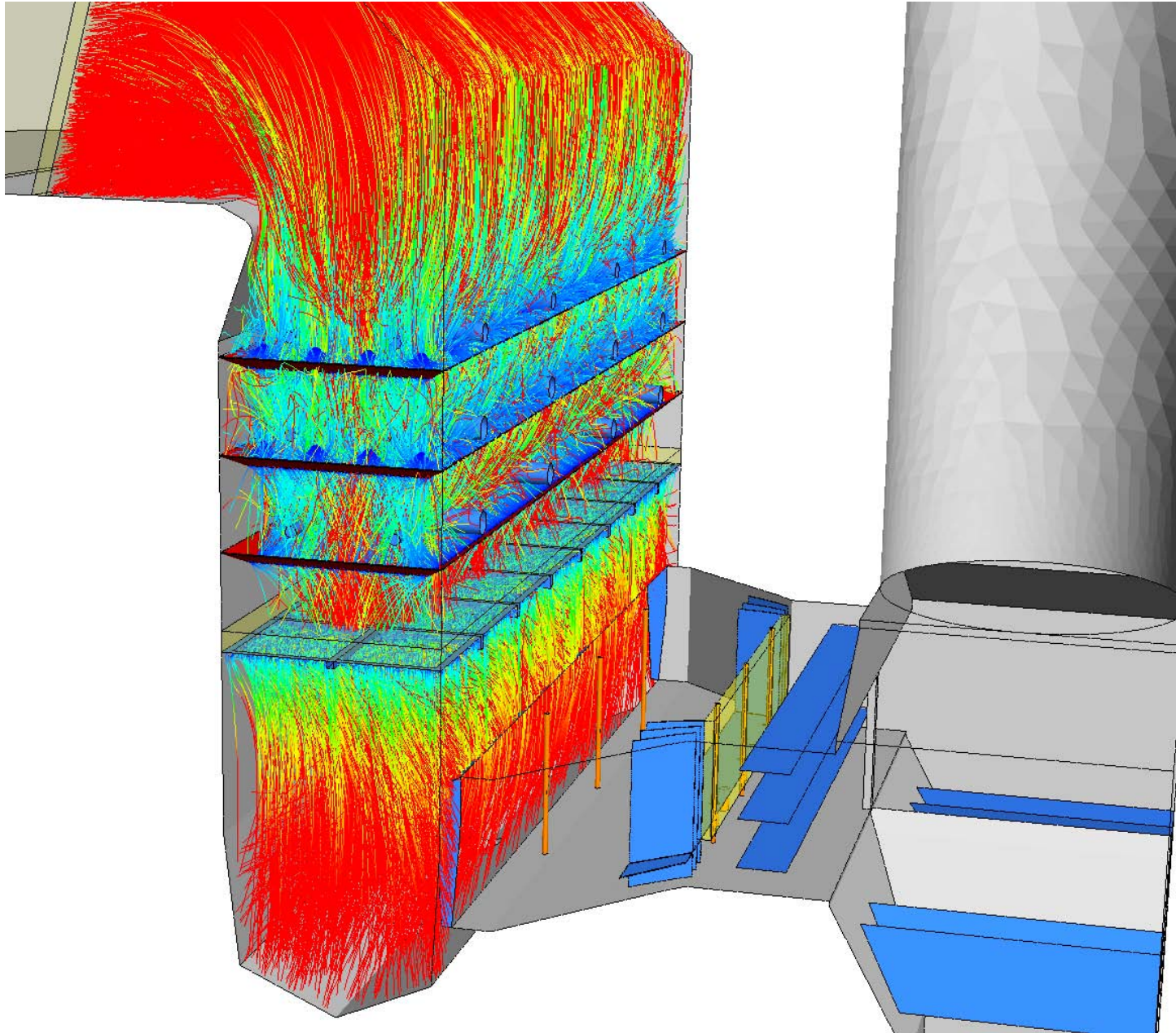


Upgrade Approach and performance

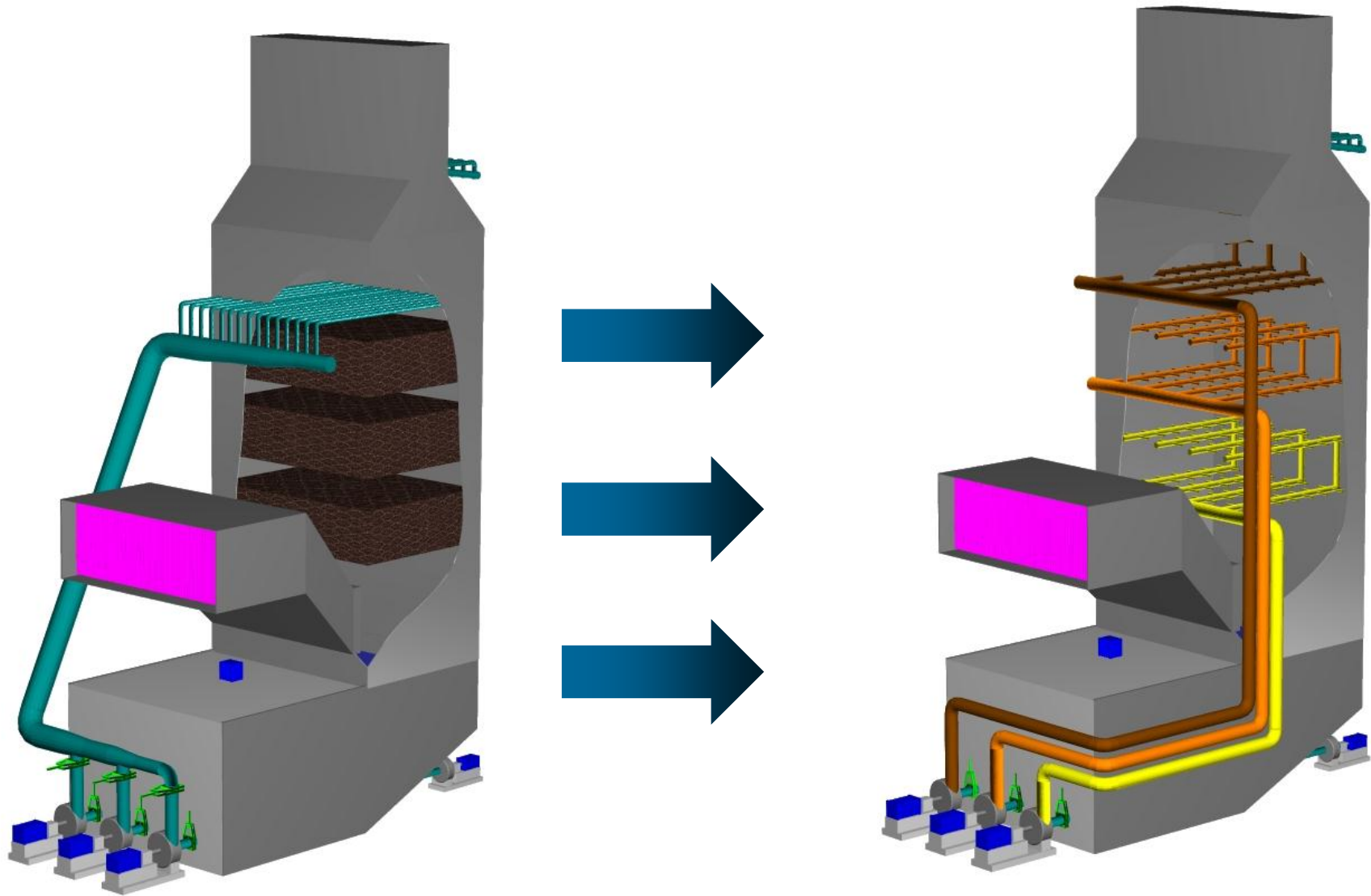
- Background
 - Riley scrubber
 - 1980
 - Medium sulfur
- Approach
 - New recycle pumps
 - Hexagonal tray
 - Spray header
 - DHC spray nozzles
 - 15 degrees slanted mist eliminator
- Performance
 - Increased SO₂ removal from 50 percent to 98 percent
 - High quality gypsum



Slurry Droplet Trajectories

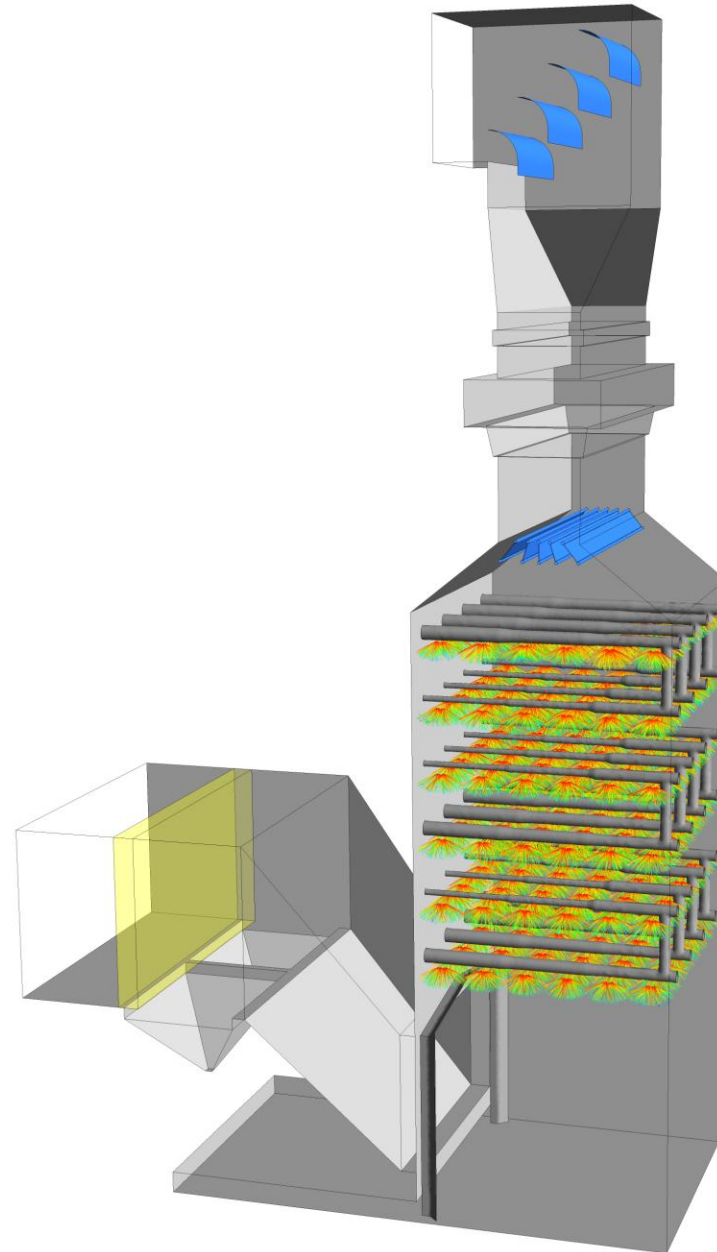


Co-current Packed Scrubber



Upgrade Approach and performance

- Background
 - MHI Scrubber
 - 1975
 - High sulfur coal
- Approach
 - New recycle pumps
 - Replaced packing with co-current spray headers
 - DHC spray nozzles
 - Two-stage mist eliminator
 - Forced Oxidation
- Performance
 - Increased SO₂ removal from 90 percent to 99 percent
 - High quality gypsum
 - Pressure rise



Inlet Duct Gas Distribution

